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Amended Claims

- 1. Process for separation of a monomer comprising at least one double bond from a composition Z comprising said monomer and at least 0,001 wt-% water as one impurity which is different to said monomer, comprising the steps:
 - bringing said composition Z into contact with an additive, wherein said additive has
 - -- a melting point of at most 150 °C and
 - -- a vapour pressure of at most 1 mbar at a temperature of 20 °C, by forming a separation phase as well as
 - separating said monomer from said separation phase.
- 2. Process according to claim 1, with said additive comprising at least
 - i. a ionic liquid or
 - ii. a highly branched polymer or
 - iii. a mixture of at least two thereof.
- 20 3. Process according to claim 2, wherein said highly branched polymer has at least 3 repeating units per molecule, each comprising at least three possible

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binding sites, wherein at least three of said repeating units are each attached via at least three possible binding sites to at least three other repeating units.

- 4. Process according to claim 2, wherein said highly branched polymer has at least 3 repeating units per molecule, which have respectively at least three possible binding sites, wherein at least three of said repeating units have at least two possible binding sites.
- 5. Process according to claim 2, wherein said ionic liquid is liquid at a temperature of 20 °C and has a viscosity in a range from 1 to 10,000 mPa×sec.
 - 6. Process according to one of the foregoing claims, wherein the selective separation of said monomer from said composition Z which has been brought into contact with said additive occurs by distillation or by extraction or crystallisation or a combination of at least two thereof.
 - 7. Process according to on of the foregoing claims, wherein said additive is brought into contact with said composition Z, said additive being in a quantity in a range from 0.01 to 95 wt.% based on the total weight of the additive and the composition Z.
 - 8. Process according one of the foregoing claims, wherein said additive is recycled.

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- 9. Process according to claim 6, wherein said recycling of said additive occurs by a separation step requiring energy input.
- 5 10. Process according to one of the foregoing claims, wherein said monomer is (meth)acrylic acid.
 - 11. Process according to on of the foregoing claims, wherein said composition Z is an acrylic acid-comprising composition ZAA based on
 - (γ1) 5 to 99.994 wt.% monomeric acrylic acid, and as impurity
 - $(\gamma 2)$ at least 0.001 wt.% of at least one acrylic acid oligomer,
 - $(\gamma 3)$ at least 0.001 wt.% acetic acid,
 - $(\gamma 4)$ at least 0.001 wt.% propionic acid,
 - $(\gamma 5)$ at least 0.001 wt.% of at least one aldehyde,
 - (γ6) at least 0.001 wt.% maleic acid or maleic acid anhydride,
 - (γ 7) at least 0.001 wt.% of at least one by-product which is different from the components (γ 1) to (γ 6) and
 - $(\gamma 8)$ a residual quantity of a fluid and

wherein the sum of the components (γ 1) to (γ 8) amounts to 100 wt.%.

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- 12. Process according to one of the foregoing claims, wherein at least one impurity is depleted.
- 13. A device for synthesis of a monomer comprising the following components in fluid-conducting assembly:
 - (δ1) a monomer synthesis unit (1) comprising a gas phase monomer synthesis unit (1a) with a quench unit (2) following said gas phase monomer synthesis unit (1a), or
 - (δ 2) a liquid phase monomer synthesis unit (1b),
- (δ3) optionally a first purification unit (3) following said liquid phase
 monomer synthesis unit (1b) or said quench unit (2),
 - $(\delta 4)$ a first monomer separation unit (4), comprising as components:
 - (δ4_1) a conduit for a monomer-comprising composition Z (5) connected with said liquid phase monomer synthesis unit
 (1b) or with said quench unit (2) or with said optionally present first purification unit (3),
 - $(\delta 4_2)$ an additive conduit (6),
 - (δ4_3) a contact region (7) which receives the conduit for a monomer-comprising composition conduit (5) and said additive conduit (6),
 - (δ4_4) a conduit (8) exiting said contact region (7) for separated monomer.

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- ($\delta 5$) a recycling unit (12) for the additive, which on its part comprises the following components:
 - (δ5_1) an inlet (13) for a composition comprising the additive, which is connected in fluid-conducting manner to a separating element (14),
 - (δ5_2) exiting said separating element (14), an outlet (15) for said additive, which is connected in fluid-conducting manner to said additive conduit (6) or said contact region (7),
 - (δ5_3) exiting said separating element (14), an outlet (16) for said monomer, which is connected in fluid-conduction manner with said conduit (8),
- (δ6) exiting said contact region (7), an inlet (13) which is connected with said recycling unit (12).
- 15 14. Use of an additive which has
 - a melting point of at most 100 °C at a pressure of 1 bar and
 - a vapour pressure of at most 1 mbar at 20 °C,

as separation aid for the separation of at least one monomer comprising at least one double bond from monomer-comprising compositions which comprise at least 0,001 wt.% water as impurity.